

Large Scale Container

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# Migration and Reaction of Iron oxide NP (Goethite) in the Large Scale VEGAS Container

Kumiko Miyajima<sup>1</sup>, Jürgen Braun<sup>1</sup>, Rainer Meckenstock<sup>2</sup> <sup>1</sup>VEGAS, University of Stuttgart, <sup>2</sup>University of Duisburg-Essen



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- **Transport of Particles**
- The final distribution of the particles injection was confirmed by after optical observation of the magnitude brownish color in the liquid of samples. The range of the color was ranked from 0 to 4 (4 darkest).
- Goethite particles were transported in the target zone of ROT 1.5 m with sufficient concentration. From the

### Artificial Aquifer in the Large Scale **VEGAS** Container

- Size: L/B/H = 9.0/6.0/4.5 m
- Layered heterogeneous sand aquifer  $(K = 4 \times 10^{-4} \text{ and } 4 \times 10^{-3} \text{ m/s})$
- Water table: 3.7 m
- Average seepage velocity: 0.42 m/d
- 380 Sampling ports: 378 in the aquifer, 2 in/outflow

### LNAPL Plume Zone (Toluene)

- Plume cross-sectional area: 4.0 m<sup>2</sup> in the center of the aquifer (red colored area of right schematic image)
- Toluene dosing rate  $\approx$  1.6 g/h  $(\sim 400 \text{ mg/L x 4 L/h})$
- Toluene concentration in plume ≈ 70.0 mg/L

# **Goal of Experiment**

### **Remediation of Toluene Plume Zone**

Enhancement of natural attenuation of toluene by goethite NP

### **Target Transport/Deposition of NP in Toluene Plume Zone**

- Distance of deposition of NP: r = 1.5 m $\bullet$
- Mass of deposition of NP: Based on the stoichiometry 12.0 kg Goethite to treat 5.0 kg Toluene (in three months, the mass of toluene delivered by the plume to the injection zone amounts to approx.  $m_{Tol} \approx 5.0$  kg (plume crosssectional area = 4.0 m<sup>2</sup>, v = 0.42 m/d,  $c_{Tol} \approx 70.0$  mg/L)).



distribution of the level 5 and 6, the injected particles were transported downward and downstream during and after the injection. Maximum transport distance was observed to be 4.3 m from the injection well.

# **Toluene Concentration Distribution in LSC**

Before the NP injection, most of the toluene was transported in the upper layer; after the injection, plume pathway changed and more toluene was observed in the middle layer.



Remediation

Injection position



Conditions/restraints

 $Q_{max} \sim 1.0 \text{ m}^{3}/\text{h}$ , (unconfined aquifer)

Water table rise max ~ 0.8 m (shallow injection depth, 0.8 - 3.0 m BGL)

# **Injection Set-up**

Boundary Condition	for Goethite NP		Impeller pump
Injection Method	Gravity Injection	~	$[ \\ \Rightarrow ] \longrightarrow () \\ () \\ () \\ () \\ () \\ () \\ () \\ ()$
Injection Well	4" ID with 2.2 m full screen		NP suspension NP suspension, tank, 1m <sup>3</sup> 20 g/L, 700 L/h
Qinjektion	0.7 m³/h		<
C <sub>NP</sub> (Goethite)	20 g/L		
Volumne of Injection	6 m³		
Mass of NP	120 kg		
Depth of Injection	0.8 m – 3.0 m BGL		

# **Injection Result**

To well

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During this time interval, 1394 g of TIC was produced due to toluene degradation. During the same time interval, toluene mass flux in the outflow of the container decreased from 1.2 g/h to 0.6 g/h, hence 1440 g Toluene (15.6 Mol) was degraded.

After the injection of goethite NP a distinct increase in  $\dot{m}_{TIC}$  and

decrease of  $\dot{m}_{tolu}$ , hence increase of biodegradation can be observed.

However, this increase in biodegradation lasted for approx. 100 days

(or less) only (red line) (between day 200 and day 300 in graph).

Mol Toluene ( $C_7H_8$  = 92.14 g/Mol) needs 36 electrons to be degraded, so  $36 \times 1440/92.14 = 562$  electrons are necessary for the remediation of 1440 g toluene. If these electrons were provided by Goethite only (FeO(OH) = 88.8 g/Mol) then 88.8 \* 562 = 49,905 g ~ 50 kg of Goethite was utilized.





6 m<sup>3</sup> (120 kg Goethite) in 8.5 h **Injektion Rate:** 0.7 m<sup>3</sup>/h (Goal 0.7 m<sup>3</sup>/h) Water Table Rise: max. 0.72 m

**Injected Volume:** 

<sup>1</sup>Kumiko Miyajima, Pfaffenwaldring 61, Stuttgart, Germany, <u>kumiko.miyajima@iws.uni-stuttgart.de</u> <sup>1</sup>Jürgen Braun, Pfaffenwaldring 61, Stuttgart, Germany, juergen.braun@iws.uni-stuttgart.de <sup>2</sup>Rainer Meckenstock, Universitätsstr. 5, Essen, Germany, rainer.meckenstock@uni-due.de



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